

Lecture-Ten

Boundary Layer Equations

1- Von Karman Integral Equation.

From the 2nd law of Newton's and momentum equation for a C.V as shown in Fig.(1) the following equations can be written

$$\sum F = \frac{d}{dt} \int_{c.v} \rho \, \vec{V} dV + \int_{c.s} \rho \vec{V} (\vec{V}.n) dA.$$

$$\sum F_x = \rho \left(u + \frac{\partial u}{\partial x} dx \right)^2 dy - \rho u^2 dy + \rho \left(v + \frac{\partial v}{\partial y} dy \right) \left(u + \frac{\partial u}{\partial y} dy \right) dx - \rho u \, v dx$$

$$\sum F_x = \rho \left[u^2 + 2u \frac{\partial u}{\partial x} dx + \left(\frac{\partial u}{\partial x} dx \right)^2 \right] dy - \rho u^2 dy + \rho v u dx + \rho v \frac{\partial u}{\partial y} dy dx + \rho u \frac{\partial v}{\partial y} dy dx + \rho \frac{\partial v}{\partial y} \cdot \frac{\partial u}{\partial y} (dy)^2 * dx - \rho u v dx$$

$$\sum F_x = \rho \left(2u \frac{\partial u}{\partial x} + u \frac{\partial v}{\partial y} + v \frac{\partial u}{\partial y} \right) dy dx$$

After disregarding second – order terms & $\frac{\partial v}{\partial v} = -\frac{\partial u}{\partial x}$ from C.E.

$$\therefore \sum F_{x} = \rho \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) dx dy \tag{1}$$

The summation of forces on C.V may be written as

$$\sum F_{x} = p \, dy - \left(p + \frac{\partial p}{\partial x} \, dx\right) dy + \left(\tau_{x} + \frac{\partial \tau_{x}}{\partial y} \, dy\right) dx - \tau_{x} dx$$

$$\sum F_{x} = p \, dy - p dy - \frac{\partial p}{\partial x} dx dy + \tau_{x} dy + \frac{\partial \tau_{x}}{\partial y} dy dx - \tau_{x} dx$$

$$\sum F_{x} = \left(-\frac{\partial p}{\partial x} + \frac{\partial \tau_{x}}{\partial y}\right) dx dy \tag{2}$$

Equating Eq's (1 & 2)

$$\rho \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) dx dy = \left(-\frac{\partial p}{\partial x} + \frac{\partial \tau_x}{\partial y} \right) dx dy \tag{3}$$

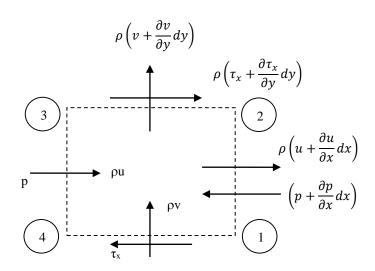


Figure 1: Distribution of pressure forces on control volume.



The shear stress is very nearly equal to

$$\tau_x = \mu \frac{\partial u}{\partial y}$$
; Substituting in Eq.(3) gives

$$\rho \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \left(\frac{\mu}{\rho} \right) \frac{\partial^2 u}{\partial y^2}$$
 (4)

Table 1: Masses and momentum fluxes on control volume faces

Surface	Mass flux	Flux of x-momentum
(1-2)	$\rho\left(u + \frac{\partial u}{\partial x} dx\right) dy$	$\rho \left(u + \frac{\partial u}{\partial x} dx \right)^2 dy$
(3-4)	ρu dy	$ ho u^2 dy$
(2-3)	$\rho\left(v + \frac{\partial v}{\partial y} dy\right) dx$	$\rho \left(v + \frac{\partial v}{\partial y} dy \right) \left(u \frac{\partial u}{\partial y} dy \right) dx$
(4-1)	ρv dx	ρν udx

From the Integral method of momentum equation for Von Karman integral as follows

$$\int_0^h \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) dy = \int_0^h -\frac{1}{\rho} \frac{dp}{dx} dy + \int_0^h v \frac{\partial^2 u}{\partial y^2} dy$$
 (5)

Where h is an undefined distance from the wall to outside the boundary layer. Integrating the second term in the integral by parts, we have

$$\left[\int_0^h v \frac{\partial u}{\partial y} dy\right] = \left[vu\right]_0^h - \int_0^h u \frac{\partial v}{\partial y} dy - - - - (a)$$

From C.E, v at y=h is given by;

$$v = \int_0^h \frac{\partial v}{\partial y} dy = -\int_0^h \frac{\partial u}{\partial x} dy \qquad \qquad ----(b)$$

Substitute Eq. (b in a) and $u = U_{\infty}$ at y = h

$$\left[\int_0^h v \, \frac{\partial u}{\partial y} \, dy\right] = -U_\infty \, \int_0^h \frac{\partial u}{\partial x} \, dy + \int_0^h u \, \frac{\partial u}{\partial x} \, dy \quad ----(c)$$

$$\underline{CASE(A)} \ \frac{\partial p}{\partial x} = 0$$

Substitute Eq. (c) in Eq's (8.9& 8.10) and neglecting $\frac{\partial p}{\partial x} = 0$

$$\int_{0}^{h} \rho \left(u \frac{\partial u}{\partial x} + u \frac{\partial u}{\partial x} - U_{\infty} \frac{\partial u}{\partial x} \right) dy = -\tau_{0}$$

$$\int_{0}^{h} \rho \left(2u \frac{\partial u}{\partial x} - U_{\infty} \frac{\partial u}{\partial x} \right) dy = -\tau_{0}$$

$$-----(e)$$

$$\int_{0}^{h} \rho \left(U_{\infty} \frac{\partial u}{\partial x} - 2u \frac{\partial u}{\partial x} \right) dy = \tau_{0}$$

$$-----(f)$$

$$\int_0^h \rho \left(U_\infty \frac{\partial u}{\partial x} - 2u \frac{\partial u}{\partial x} \right) dy = \tau_0 \qquad ---- (f)$$

Since
$$\frac{\partial u^2}{\partial x} = 2u \frac{\partial u}{\partial x}$$

$$\int_0^h \rho\left(\left(U_\infty \frac{\partial u}{\partial x}\right) - \frac{\partial}{\partial x}(u^2)\right) dy = \tau_0$$

$$\tau_0 = \rho \frac{d}{dx} \int_0^h u \left(U_{\infty} - u \right) dy \qquad since \ h = \delta$$

$$\tau_0 = \rho \frac{d}{dx} \int_0^\delta u \, (\, \mathrm{U}_\infty - u) dy$$

$$\frac{\tau_0}{\rho U_{\infty}^2} = \frac{d}{dx} \int_0^{\delta} \frac{u}{U_{\infty}} \left(1 - \frac{u}{U_{\infty}} \right) dy \tag{6}$$



$$\frac{\tau_0}{\rho U_{\infty}^2} = \frac{d\theta}{dx} \tag{7}$$

Since
$$\theta = \int_0^\delta \frac{u}{U_m} \left(1 - \frac{u}{U_m} \right) dy$$
 (8)

Eq. (8) is the Von Karman equation without pressure gradient dp/dx=0

$$\underline{CASE(B)}$$
 $\frac{\partial p}{\partial x} \neq 0$

When the pressure gradient in Eq's (4 or 5) is included and from adding it in Eq. (e) as followss $\frac{dU_{2}}{dt} = \frac{dU_{2}}{dt} = \frac{dU_{2}}{$

$$-\frac{1}{\rho}\frac{dp}{dx} = U_{\infty}\frac{dU_{\infty}}{dx}$$
 from Bournalli's Equation

$$\operatorname{Now} \int_0^h \rho \left(-\operatorname{U}_{\infty} \frac{\partial u}{\partial x} + 2u \frac{\partial u}{\partial x} - \operatorname{U}_{\infty} \frac{dU_{\infty}}{dx} \right) dy = -\tau_0 \tag{9}$$

$$\frac{\partial}{\partial x} (u U_{\infty}) = U_{\infty} \frac{\partial u}{\partial x} + u \frac{\partial U_{\infty}}{\partial x}$$

$$U_{\infty} \frac{\partial u}{\partial x} = \frac{\partial}{\partial x} (u U_{\infty}) - u \frac{\partial U_{\infty}}{\partial x}$$
 Substituted in Eq. (9) after multiply by (-1)

$$\int_0^h \left[2u \frac{\partial u}{\partial x} - U_{\infty} \frac{\partial U_{\infty}}{\partial x} + u \frac{\partial U_{\infty}}{\partial x} - \frac{\partial}{\partial x} (u U_{\infty}) \right] dy = -\frac{\tau_0}{\rho}$$

In above eqn. $2u\frac{\partial u}{\partial x} = \frac{\partial u^2}{\partial x}$

$$\int_0^h \frac{\partial}{\partial x} \left[u \left(u - U_{\infty} \right) \right] dy - \frac{dU_{\infty}}{dx} \int_0^h \left(U_{\infty} - u \right) dy = -\frac{\tau_0}{\rho}$$

$$\theta = \int_0^{\delta} \frac{u}{U_m} \left(1 - \frac{u}{U_m} \right) dy$$

$$\delta_d = \int_0^{\delta} \left(1 - \frac{u}{U}\right) dy$$

$$\therefore \frac{\tau_0}{\rho} = \frac{d}{dx} (U_{\infty}^2 \theta) + U_{\infty} \delta_d \frac{dU_{\infty}}{dx}$$

$$\frac{\tau_0}{\rho} = U_{\infty}^2 \frac{d\theta}{dx} + \theta * 2U_{\infty} \frac{dU_{\infty}}{dx} + U_{\infty} \delta_d \frac{dU_{\infty}}{dx}$$

$$\frac{\tau_0}{\rho} = U_{\infty}^2 \frac{d\theta}{dx} + (2\theta + \delta_d) U_{\infty} \frac{dU_{\infty}}{dx}$$
 (10)

We assume

$$C_f = \frac{\tau_0}{\frac{1}{2}\rho U_{\infty}^2}$$
 and $H = \frac{\delta_d}{\theta}$

 C_f is the friction factor and H is the shape factor.

$$\therefore \frac{c_f}{2} = \frac{d\theta}{dx} + \theta(2 + H) \frac{1}{U_{\infty}} \frac{dU_{\infty}}{dx}$$
 (11)

From Eq's (10 and 11) the case of $\frac{dp}{dx} = 0 \& \frac{dU_{\infty}}{dx} = 0$

No gradient of pressure along the x-axis

$$\frac{\tau_0}{\rho U_{co}^2} = \frac{d\theta}{dx} = \frac{1}{2} cf \tag{12}$$

2- Approximate Solution to the Laminar B.L.

We have four conditions that proposed velocity profile should satisfy on flat plat with zero pressure gradients.

$$u = 0$$
 at $y = 0$

$$u = U_{\infty} at y = \delta$$

$$\frac{\partial u}{\partial x} = 0$$
 at $y = \delta$



$$\frac{\partial^2 u}{\partial y^2} = 0 \ at \ y = 0$$

Let $\frac{u}{U_{\infty}} = A + By + Cy^2 + Dy^3$ is a cubic polynomial will satisfy the four conditions.

From above conditions
$$\begin{array}{lll} & \text{At } y{=}0 \text{ , } u{=}0 \\ & \frac{u}{U_{\infty}} = 0 = A \\ & & -{---}{-}(a) \end{array} \\ & \text{At } y = \delta \qquad u = U_{\infty} \\ & \frac{U}{U_{\infty}} = 1 = B\delta + C\delta^2 + D\delta^3 \qquad -{---}(b) \\ & \text{At } y = \delta \qquad \frac{\partial u}{\partial y} = 0 \\ & \frac{\partial u}{\partial y} = B + 2cy + 3Dy^2 \\ & B + 2C\delta + 3D\delta^2 = 0 \qquad -{---}(c) \\ & \text{At } y{=}0 \\ & \frac{\partial^2 y}{\partial y^2} = 0 = 2C + 6Dy - {---} C = 0 \qquad -{--}(d) \\ & \text{From Eq. (c)} \qquad \Rightarrow B = -3D\delta^2 \qquad -{---}(e) \\ & \text{From Eq. (b)} \qquad B = \frac{1}{\delta} - D\delta^2 \qquad -{---}(f) \end{array}$$

$$\frac{\partial y}{\partial y^2} = 0 = 2C + 6Dy - \cdots \rightarrow C = 0 \qquad ----(d)$$

From Eq. (c)
$$\Rightarrow B = -3D\delta^2$$
 $----(e)$

From Eq. (b)
$$B = \frac{1}{\delta} - D\delta^2$$
 $----(f)$

Equating (e & f)

$$-3D\delta^2 = \frac{1}{\delta} - D\delta^2 \qquad --- \rightarrow D = -\frac{1}{2\delta^3} \; ; \quad B = \frac{3}{2\delta}$$

Hence a good approximation for the velocity profile in a laminar flow is

$$\frac{u}{U_{\infty}} = \frac{3}{2} \left(\frac{y}{\delta} \right) - \frac{1}{2} \left(\frac{y}{\delta} \right)^3$$

Let us now use this velocity profile to find $\delta(x)$ and $\tau_0(x)$. From Von Karman's integral Eq's (6 & 7)

$$\frac{\tau_0}{\rho U_{\infty}^2} = \frac{d}{dx} \int_0^{\delta} \frac{u}{U_{\infty}} \left(1 - \frac{u}{U_{\infty}} \right) dy$$

Assume the velocity take the following form $\frac{u}{U_m} = \frac{3y}{2\delta} - \frac{y^3}{2\delta^3}$ in the B.L. Calculate the thickness and the wall shear.

$$\frac{\tau_{0}}{\rho U_{\infty}^{2}} = \frac{d}{dx} \int_{0}^{\delta} \frac{u}{U_{\infty}} \left(1 - \frac{u}{U_{\infty}} \right) dy$$

$$\frac{\tau_{0}}{\rho U_{\infty}^{2}} = \frac{d}{dx} \int_{0}^{\delta} \left(\frac{3}{2} \frac{y}{\delta} - \frac{y^{3}}{2\delta^{3}} \right) \left(1 - \frac{3y}{2\delta} + \frac{y^{3}}{2\delta^{3}} \right) dy$$

$$\frac{\tau_{0}}{\rho U_{\infty}^{2}} = \frac{d}{dx} \int_{0}^{\delta} \left(\frac{3}{2} \frac{y}{\delta} - \frac{9y^{2}}{4\delta^{2}} + \frac{3y^{4}}{4\delta^{4}} - \frac{y^{3}}{2\delta^{3}} + \frac{3y^{4}}{4\delta^{4}} - \frac{y^{6}}{4\delta^{6}} \right) dy$$

$$\frac{\tau_{0}}{\rho U_{\infty}^{2}} = \frac{d}{dx} \int_{0}^{\delta} \left(\frac{3}{2} \frac{y}{\delta} - \frac{9y^{2}}{4\delta^{2}} + \frac{6y^{4}}{4\delta^{4}} - \frac{y^{3}}{2\delta^{3}} - \frac{y^{6}}{4\delta^{6}} \right) dy$$

$$\frac{\tau_{0}}{\rho U_{\infty}^{2}} = \frac{d}{dx} \left[\frac{3y^{2}}{4\delta} - \frac{9y^{3}}{12\delta^{2}} + \frac{6y^{5}}{20\delta^{4}} - \frac{y^{4}}{8\delta^{3}} - \frac{y^{7}}{28\delta^{6}} \right]_{0}^{\delta}$$

$$\frac{\tau_{0}}{\rho U_{\infty}^{2}} = \frac{d}{dx} \left[\frac{3}{4} \delta - \frac{9}{12} \delta + \frac{6}{20} \delta - \frac{\delta}{8} - \frac{\delta}{28} \right]$$

$$\frac{\tau_{0}}{\rho U_{\infty}^{2}} = \frac{d\delta}{dx} \left(0.1392 \right) = 0.1392 \frac{d\delta}{dx}$$

$$\therefore \tau_{0} = 0.1392 \rho U_{\infty}^{2} d\delta / dx$$



At the wall we know that $\tau_0 = \mu \frac{\partial u}{\partial y}\Big|_{y=0}$ or using the cubic profile

$$\frac{\partial u}{\partial y}\Big|_{y=0} = B + 2Cy + 3Dy^2 = B = \left(\frac{3}{2\delta}\right)U_{\infty}$$

$$\therefore \tau_0 = \mu\left(U_{\infty}\frac{3}{2\delta}\right)$$
(14)

Equating the foregoing expression (13 & 14) for $\tau_0(x)$, we find that

$$0.139\rho U_{\infty}^{2} \frac{d\delta}{dx} = \mu \left(U_{\infty} \frac{3}{2\delta} \right)$$

$$\delta d\delta = \frac{\frac{3}{2}\mu}{0.139\rho U_{\infty}} dx = 10.8 \frac{\nu}{U_{\infty}} dx$$
(15)

From using at $\delta = 0$ at x = 0 (the leading edge) Eq. (15) is integrated to give

$$\delta = 4.65 \sqrt{vx/U_{\infty}} \quad \text{multiply by } \frac{\sqrt{x}}{\sqrt{x}}$$

$$\delta = 4.65 \frac{x}{\sqrt{Re_x}} \tag{16}$$

Where Re_x is the local Reynolds number. Substituted Eq. (16) in Eq.(14) giving the wall shear as

$$\tau_0 = 0.323 \,\rho \,\mathrm{U}_{\infty}^2 \,\sqrt{\frac{\nu}{x \,\mathrm{U}_{\infty}}}$$

$$\tau_0 = \frac{0.323 \rho \,\mathrm{U}_{\infty}^2}{\sqrt{Re_x}} \tag{17}$$

The shearing stress is made dimensionless by dividing by $\frac{1}{2} \rho U_{\infty}^2$. The local skin friction coefficient C_f

$$C_f = \frac{\tau_0}{\frac{1}{2}\rho U_\infty^2} = \frac{0.646}{\sqrt{U_\infty \frac{x}{\nu}}} = \frac{0.646}{\sqrt{Re_x}}$$
 (18)

If the wall shear is integrated over the length L, the result per unit width is the drag force.

$$F_{D} = \int_{0}^{L} \tau_{0} dx = 0.646 \, \rho U_{\infty} \sqrt{U_{\infty} \, L \nu} \quad \text{Where } \tau_{0} \text{ from Eq. (17)}$$

$$F_{D} = \frac{0.646 \, \rho U_{\infty}^{2} L}{\sqrt{Re_{L}}} \qquad (19)$$

$$\text{Or } F_{D} = \int_{0}^{L} \tau_{0} \, dx = \tau_{0} . L = C_{F} . \frac{1}{2} \rho U_{\infty}^{2} . L \quad \text{since } \tau_{0} \text{ from Eq. (18)}$$

$$\therefore C_{F} = \frac{F_{D}}{\frac{1}{2} \rho U_{\infty}^{2} . L} = \frac{0.646 \, \rho U_{\infty}^{2} . L}{\frac{1}{2} \rho U_{\infty}^{2} . L \sqrt{Re_{L}}} = \frac{1.292}{\sqrt{Re_{L}}} \qquad (20)$$

Where Re_L is the Reynolds number at the end of flat plate.

Ex.1

Assume a parabolic velocity profile and calculate the B.L thickness and the wall shear. Compare with those calculate above.

Sol.

The parabolic velocity profile is assumed to be

$$\frac{u}{U_{\infty}} = A + By + Cy^2$$

With three conditions

$$u = 0$$
 at $y = 0$; $u = U_{\infty}$ at $y = \delta$; $\frac{\partial u}{\partial y} = 0$ at $y = \delta$ $\therefore A = 0$
 $1 = A + B\delta + C\delta^2 = B\delta + C\delta^2$;



$$0 = B + C * 2\delta$$

Then A=0;
$$B = \frac{2}{\delta}$$
; $C = -\frac{1}{\delta^2}$. The velocity profile is

$$\frac{u}{U_{\infty}} = 2\frac{y}{\delta} - \frac{y^2}{\delta^2} - - - - - (a)$$

This is substituted into Von Karman's integral equation (6) to obtain

$$\begin{split} &\frac{\tau_0}{\rho U_{\infty}^2} = \frac{d}{dx} \int_0^{\delta} \left(\frac{2y}{\delta} - \frac{y^2}{\delta^2} \right) \left[1 - \frac{2y}{\delta} + \frac{y^2}{\delta^2} \right] dy \\ &= \frac{d}{dx} \int_0^{\delta} \left[\frac{2y}{\delta} - \frac{4y^2}{\delta^2} + \frac{2y^3}{\delta^3} - \frac{y^2}{\delta^2} + \frac{2y^3}{\delta^3} - \frac{y^4}{\delta^4} \right] dy \\ &= \frac{d}{dx} \left[\frac{2y^2}{2\delta} - \frac{4y^3}{3\delta^2} + \frac{2y^4}{4\delta^3} - \frac{y^3}{3\delta^2} + \frac{2y^4}{4\delta^3} - \frac{y^5}{5\delta^4} \right]_0^{\delta} \\ &= \frac{d}{dx} \left[\delta - \frac{4}{3} \delta + \frac{1}{2} \delta - \frac{1}{3} \delta + \frac{1}{2} \delta - \frac{1}{5} \delta \right] \\ &= \frac{d}{dx} \left[1 - \frac{4}{3} + \frac{1}{2} - \frac{1}{3} + \frac{1}{2} - \frac{1}{5} \right] \delta \\ &= \frac{d}{dx} \left(\frac{30 - 25 - 3}{15} \right) \delta = \frac{d}{dx} \frac{2}{15} \delta \\ &\therefore \tau_0 = \frac{2}{15} \rho U_{\infty}^2 \frac{d\delta}{dx} \qquad - - - - - - (b) \end{split}$$

We also use $\tau_0 = \mu \frac{\partial u}{\partial v}\Big|_{y=0}$

From Eq. (a)

$$\tau_0 = \mu \, \mathrm{U}_{\infty} \frac{2}{\delta} \qquad \qquad ---- (c)$$

Equating Eq's (b & c) we obtain

$$\frac{2}{15} \rho U_{\infty}^{2} \frac{d\delta}{dx} = \mu U_{\infty} \frac{2}{\delta}$$
$$\delta d\delta = 15 \frac{\nu}{U_{\infty}} dx$$

$$\delta d\delta = 15 \frac{v}{U_{\infty}} dx$$
 Using $\delta = 0$ at $x = 0$ after integration

$$\int_0^\delta \delta d\delta = \int_0^x 15 \frac{v}{U_\infty} \ dx$$

$$\frac{\delta^2}{2} = 15 \frac{v}{U_{co}} x$$

$$\therefore \ \delta = 5.48 \sqrt{\frac{vx}{U_{\infty}}} \qquad \qquad ----(d)$$

This is 18% higher than the value using the cubic profile, the wall shear is found to be

$$\tau_0 = \frac{2\mu U_{\infty}}{\delta}$$
 Substitute Eq. (d)

$$\tau_0 = \frac{2\mu U_{\infty}}{5.43} \sqrt{\frac{U_{\infty}}{\nu x}}$$

$$\tau_0 = 0.365 \, \rho U_{\infty}^2 \sqrt{\frac{\nu}{x \, U_{\infty}}} = \frac{0.365 \rho U_{\infty}^2}{\sqrt{Re_x}}$$

This is 13% higher than the value using the cubic velocity profile.

3- Solution of Turbulent B.L. Power – Law Form.

The power-law form is

$$\frac{u}{U_{\infty}} = \left(\frac{y}{\delta}\right)^{1/n} \qquad n = \begin{cases} 7 & Re_{x} < 10^{7} \\ 8 & 10^{7} < Re_{x} \le 10^{8} \\ 9 & 10^{8} < Re_{x} \le 10^{9} \end{cases}$$
 (21)



The Balsius formula is an empirical relation for the local friction coefficient

$$C_f = 0.046 \left(\frac{\nu}{U_{\infty}\delta}\right)^{\frac{1}{4}} \tag{22}$$

We have
$$C_f = \frac{\tau_0}{\frac{1}{2}\rho U_\infty^2}$$
 $- \rightarrow \tau_0 = C_f \frac{1}{2}\rho U_\infty^2$

$$\dot{\tau}_0 = 0.023 \,\rho U_\infty^2 \, \left(\frac{\nu}{U_\infty \delta}\right)^{1/4} \tag{23}$$

Substitute the velocity profile in Von Karman's integral Eq. 6 with $Re_x < 16^7$

$$\frac{\tau_0}{\rho U_\infty^2} = \frac{d}{dx} \int_0^\delta \left[\left(\frac{y}{\delta} \right)^{1/7} \left(1 - \left(\frac{y}{\delta} \right)^{\frac{1}{7}} \right) \right] dy$$

$$\tau_0 = \frac{7}{72} \rho U_\infty^2 \frac{d\delta}{dx} \tag{24}$$

Equating Eq's (23 & 24) for τ_0 , we find that

$$\delta^{\frac{1}{4}} d\delta = 0.237 \left(\frac{v}{U_{\infty}}\right)^{\frac{1}{4}} dx$$

Assuming a turbulent flow from the leading edge $L>>x_L$, from integration the above eqn.

$$\frac{\delta^{\frac{5}{4}}}{\frac{5}{4}} = 0.237 \left(\frac{v}{U_{\infty}}\right)^{1/4} x$$

After taking the root (4/5) and multiplied by $(x/x)^{1/5}$ gives the following

$$\delta = 0.38 \, x \, (Re_x)^{-1/5} \tag{25}$$

Substituting Eq. 8.30 for δ in to Eq. (22) we find that

$$C_f = 0.059(R_e)^{-1/5} \quad for \quad Re < 10^7$$
 (26)

The drag force =
$$F_D = \tau_0 A = C_f \frac{1}{2} \rho U_\infty^2(LW)$$
 (27)

Where W is the width of plate and C_f from Eq. (26).

Ex.2

Estimate the boundary layer thickness at the end of a 4-m-long flat surface if the free-stream velocity $U_{\infty} = 5 \frac{m}{s}$. Use atmospheric air at $30C^{\circ}$. And predict the drag force if the surface is 5m wide

- a) Neglect the laminar portion of the flow
- b) Account for the Laminar portion using $Re_{crit.} = 5 * 10^5$.

<u>Sol.</u>

a) Let us first assume turbulent flow from the leading edge. The B.L thickness is given by Eq. (25). It is $\delta = 0.38 \ x \ Re_x^{-1/5}$

$$\delta = 0.38 * 4 * \left(\frac{5*4}{1.6*10^{-5}}\right)^{-1/5} = 0.092m$$

The drag force is using Eq's (8.31 & 8.32); $Re = \frac{U_{\infty}L}{v}$

$$F_D = C_f * \frac{1}{2} \rho \mathrm{U}_\infty^2(LW) = 0.059 (Re^-)^{-1/5} * \frac{1}{2} \rho \mathrm{U}_\infty^2(L.W)$$

$$F_D = 0.059 \left(\frac{5*4}{1.6*10^{-5}} \right)^{-1/5} * \frac{1}{2} * 1.16 * 5^2 * 4 * 5 = 1.032N$$

 $Re_L = \frac{5*4}{1.6*10^{-5}} = 1.25*10^6$. Hence, the calculation is acceptable

The distance is found as follows



$$Re_{crit.} = 5 * 10^5 = \frac{U_{\infty}x_L}{v}$$

$$Re_{crit.} = 5 * 10^5 = \frac{U_{\infty}x_L}{v}$$

$$\therefore x_L = \frac{5*10^5*1.6*10^{-5}}{5} = 1.6 m$$

The B.L thickness at x_L is found from Eq. (16) with

$$\delta = 4.65 \frac{x_L}{\sqrt{Re_x}} = \frac{4.65 * 1.6}{\sqrt{5 * 10^5}} = 0.0105 \ m$$

To find the origin of turbulent flow, using equation of B.L thickness in turbulent as

$$\delta = 0.38 \, x \, (Re_x)^{-1/5} = \frac{0.38x'}{\left(\frac{U_{\infty}x}{v}\right)^{\frac{1}{5}}} = \frac{0.38x^{\frac{4}{5}}}{\left(\frac{U_{\infty}}{v}\right)^{\frac{1}{5}}}$$
$$\therefore x'^{4/5} = \frac{\delta}{0.38} \left(\frac{U_{\infty}}{v}\right)^{1/5}$$

$$\therefore x'^{4/5} = \frac{\delta}{0.38} \left(\frac{U_{\infty}}{V}\right)^{1/5}$$

where δ = the same at end of L.B

$$x' = \left(\frac{0.0105}{0.38}\right)^{5/4} \left(\frac{5}{1.6*10^{-5}}\right)^{1/4} = 0.2663m$$

The distance x_t as in figure is then

$$x_t = L - x_L + x' = 4 - 1.6 + 0.266 = 2.666M$$

To find the B.L thickness at the end of plate using Eq. 8.30

$$\delta = 0.38 \, x \, Re^{-1/5} = 0.38 * 2.666 * \left(\frac{5*2.666}{1.6*10^{-5}}\right)^{-1/5}$$

$$\delta = 0.0662m$$

The value of part (a) is 28% to high when compared with this more accurate value.

